#### AMENDMENTS TO THE CLAIMS

This listing of claims will replace all prior versions, and listings, of claims in the application:

- 1. (original) A process for producing an oil or a polyunsaturated fatty acid (PUFA), the process comprising:
  - (a) deaerating an aqueous liquid comprising cells; and
  - (b) obtaining the oil or PUFA from the cells.
- 2. (original) A process according to claim 1, wherein the cells are microbial cells.
- 3. (currently amended) A process according to claim 1 or 2, wherein the cells are heated or pasteurised after deaeration in (a) but before stage (b).
- 4. (currently amended) A process according to any preceding claim claim 1, wherein the aqueous liquid is a fermentation broth.
- 5. (currently amended) A process according to any preceding claim claim 1 which further comprises:
  - (c) extracting, purifying or isolating the oil or one or more PUFAs.
- 6. (currently amended) A process according to any preceding claim claim 1 wherein deaeration comprises:
  - a) application of vacuum (or reduced pressure);
- b) mechanical deaeration/de-gassing (stirring, vibration, use of accelerative or g-force, such as in a centrifuge or a cyclon;
- c) viscosity change (either by dilution with water or other liquid, or by increase in temperature);

- d) change in fermentation conditions, for example a reduction in airlift, air sparging or the supply of oxygen or air during fermentation, or a reduction in stirring rate;
  - e) pH change, for example by lowering the pH or acidification;
- f) filtration, for example by using a filter or membrane preferably comprising an (inert) polymer, for example PTFE;
- g) gas displacement, with an inert gas such as nitrogen, a noble gas such as helium, or steam;
- h) chemical deaeration, for example using an oxygen scavenger, for example sodium sulphite or hydrazine;
- i) time, where the aqueous liquid is allowed to rest under conditions such that oxygen or air diffuses out of the liquid;

or a combination of one or more of the methods in (a) to (i).

- 7. (currently amended) A process according to any preceding claim claim 1 wherein the deaeration is effected by reduced stirring and/or gas displacement.
- 8. (original) A process according to claim 7 wherein gas displacement is performed using a gas comprising either no oxygen or oxygen at a concentration level below atmospheric air.
- 9. (currently amended) A process according to claim 7 or 8 wherein the gas is, or comprises, nitrogen.
- 10. (currently amended) A process according to any preceding claim claim 1 wherein deaeration comprises subjecting the aqueous liquid to reduced pressure.
- 11. (original) A process according to claim 10, wherein said reduced pressure is a pressure of no more than 800 mbara, preferably no more than 600 mbara.

- 12. (currently amended) A process according to claim 10 or claim 11, wherein the aqueous liquid is deaerated using a vacuum or degassing pump, a parasol deaerator or an umbrella nozzle.
- 13. (currently amended) A process according to any preceding claim claim 1, wherein deaeration results in an  $O_2$  content in the aqueous liquid of less than 20 ppm, preferably less than 10 ppm.
- 14. (currently amended) A process according to any preceding claim claim 1, wherein deaeration results in a concentration of dissolved oxygen of less than 10 ppm, preferably less than 5 ppm, more preferably less than 2 ppm.
- 15. (currently amended) A process according to any preceding claim claim 1, wherein the process comprises subjecting the deaerated aqueous liquid to
- (i) a pressure of above 1 bara, preferably above 1.5 bara, more preferably above 2 bara; and/or
- (ii) a temperature above 60 °C, preferably above 80 °C, more preferably above 100 °C.
- 16. (currently amended) A process according to any preceding claim claim 1, wherein the cells are heated or pasteurised at a temperature above 80 °C, preferably above 90 °C, preferably above 100 °C.
- 17. (currently amended) A process according to any preceding claim 1 wherein the PUFA comprises, or oil comprises a PUFA which, is a C18, C20 or C22  $\Omega$ -3 or  $\Omega$ -6 PUFA (optionally ARA, EPA, DHA and/or GLA).
- 18. (currently amended) A process according to any preceding claim claim 1, wherein the cells are yeast, bacterial, fungal or algal cells.
- 19. (currently amended) A process according to any preceding claim claim 1, wherein the oil is a microbial or single cell oil.

- 20. (currently amended) A process according to any preceding claim claim 1, wherein (b) comprises obtaining an oil comprising a PUFA from the cells, said oil having a POV of less than 12 and/or an AnV of less than 20.
- 21. (currently amended) An oil comprising a PUFA, or a PUFA, obtained by a process according to any preceding claim claim 1.
- 22. (original) An oil according to claim 21, wherein the oil is a microbial or single cell oil.
- 23. (original) Apparatus for producing an oil or a PUFA from microbial cells, comprising:
  - (a) means for culturing or fermenting microbial cells;
- (b) means for deaerating an aqueous liquid comprising the microbial cells; and
  - (c) optionally, means for obtaining the oil or PUFA from the microbial cells.
- 24. (original) Apparatus according to claim 23 wherein (a) comprises a fermenter vessel, (b) comprises a deaerator (optionally able to apply reduced pressure) and/or (c) comprises a homogeniser and/or a centrifuge.
- 25. (currently amended) Apparatus according to claim 23 <del>or 24</del> wherein (b) comprises a vacuum or degassing pump, parasol deaerator or umbrella nozzle.
- 26. (currently amended) Apparatus according to any preceding claim claim 1, wherein (b) comprises a deaerator able to apply a pressure of less than 800 mbara, preferably less than 600 mbara.